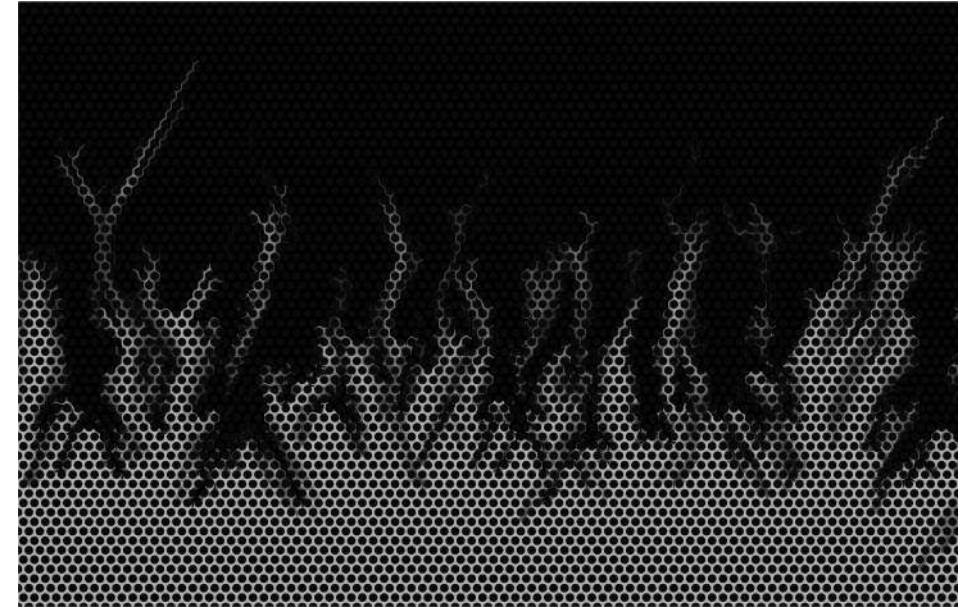
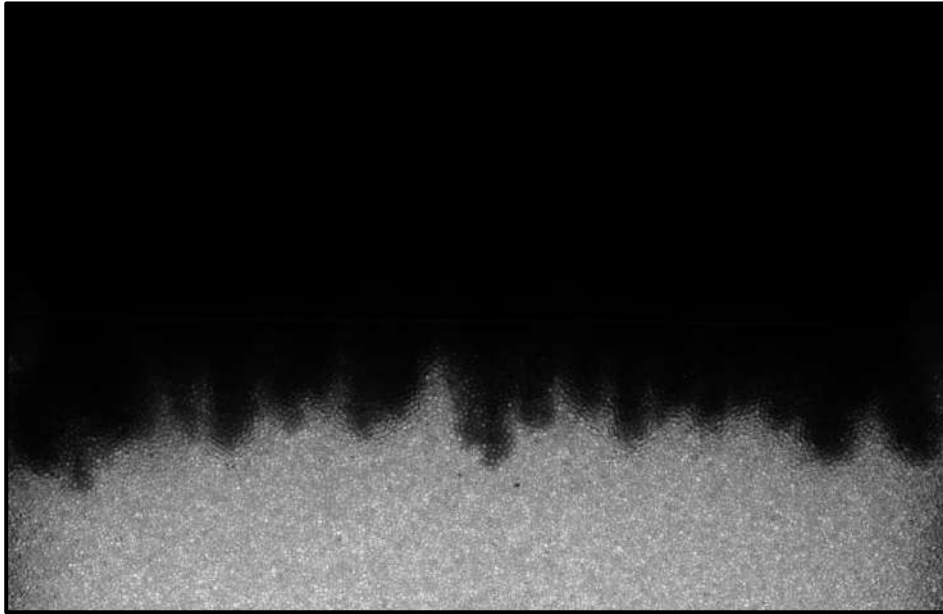


# Pore-scale simulation of convective mixing in confined media



M. De Paoli<sup>1,2</sup>, C. Howland<sup>1</sup>, R. Verzicco<sup>1,3,4</sup> & D. Lohse<sup>1,5</sup>

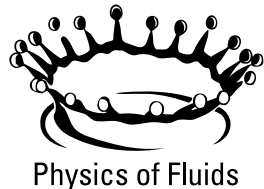
<sup>1</sup>Physics of Fluids Group, University of Twente, Enschede (The Netherlands)

<sup>2</sup>Institute of Fluid Mechanics and Heat Transfer, TU Wien, Vienna (Austria)

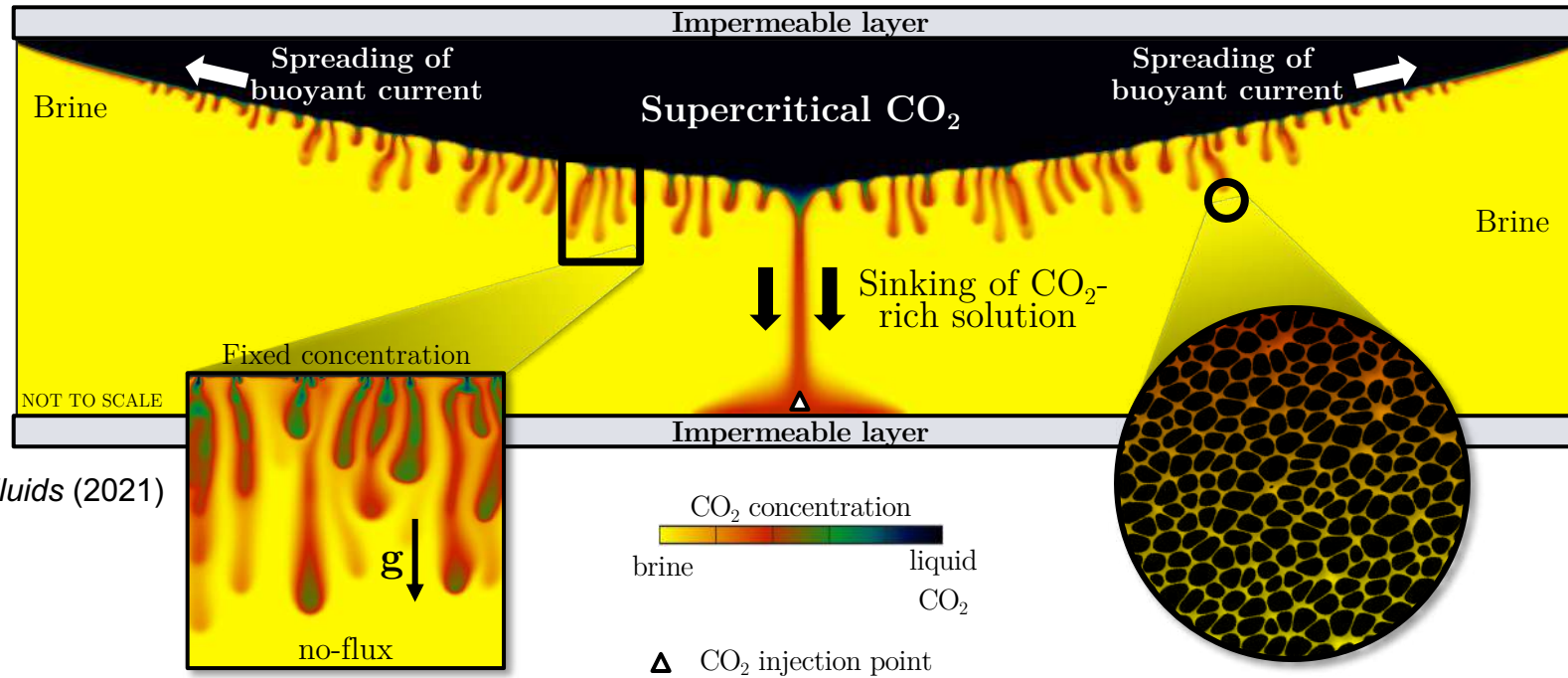
<sup>3</sup>Dipartimento di Ingegneria Industriale, University of Rome «Tor Vergata», Rome (Italy)

<sup>4</sup>Gran Sasso Science Institute, L'Aquila (Italy)

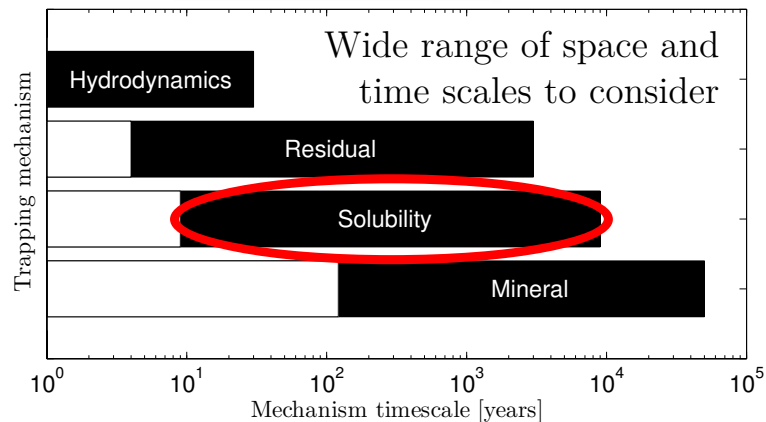
<sup>5</sup>Max Plank Institute for Dynamics and Self-Organization, Göttingen (Germany)



# Carbon Capture and Storage

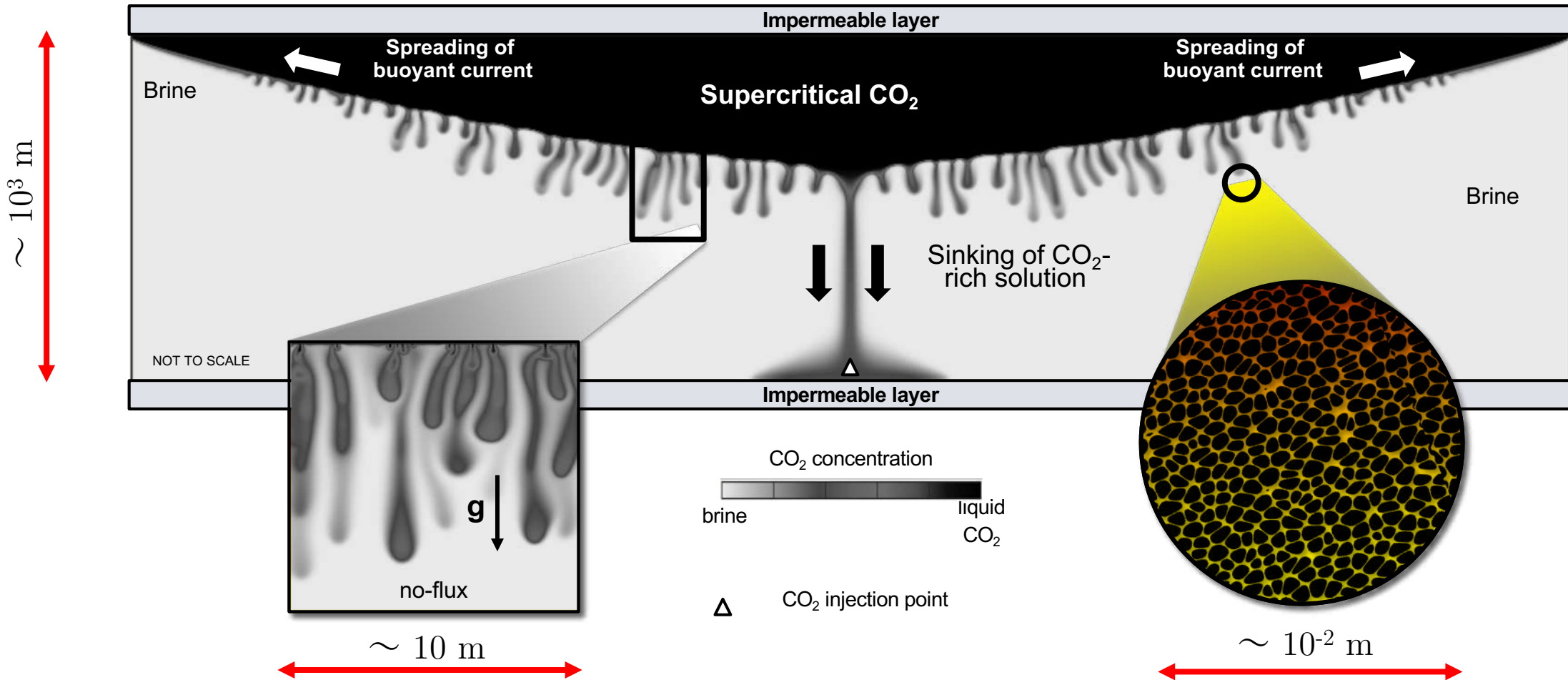


De Paoli, *Phys. Fluids* (2021)



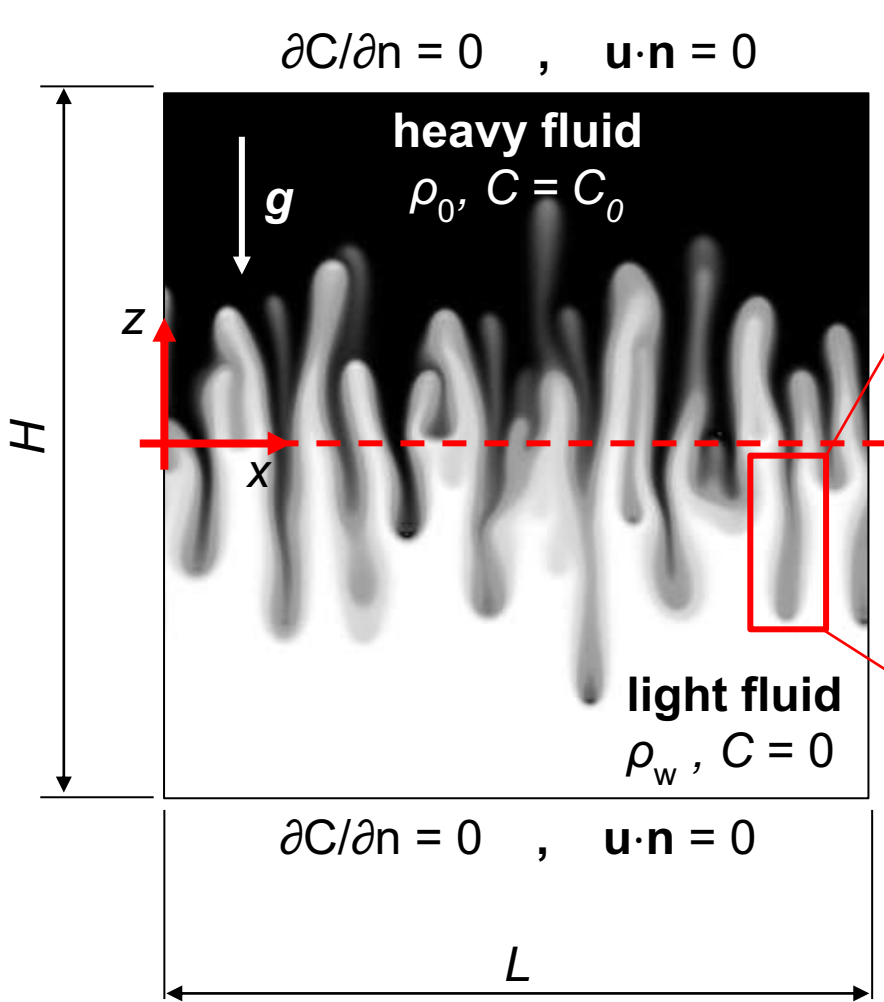
MacMinn et al., *Geophys. Res. Lett.* (2013)

# Convection in complex multiphase and multiscale systems

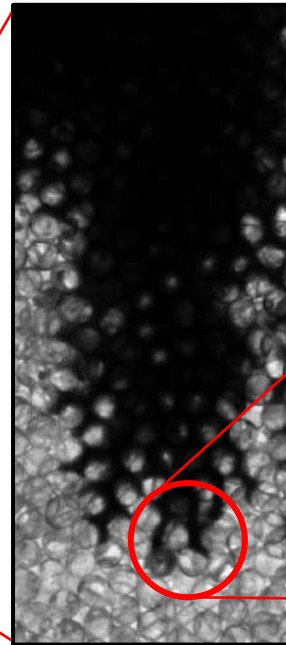


De Paoli, *Phys. Fluids* (2021)

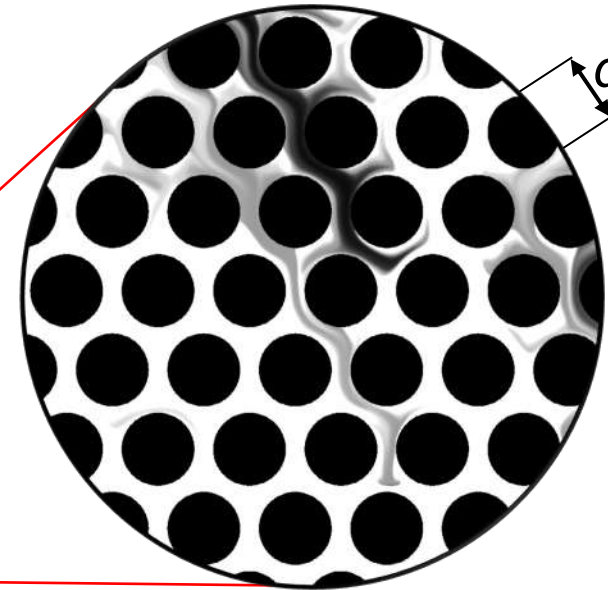
# Flow configuration



experiments



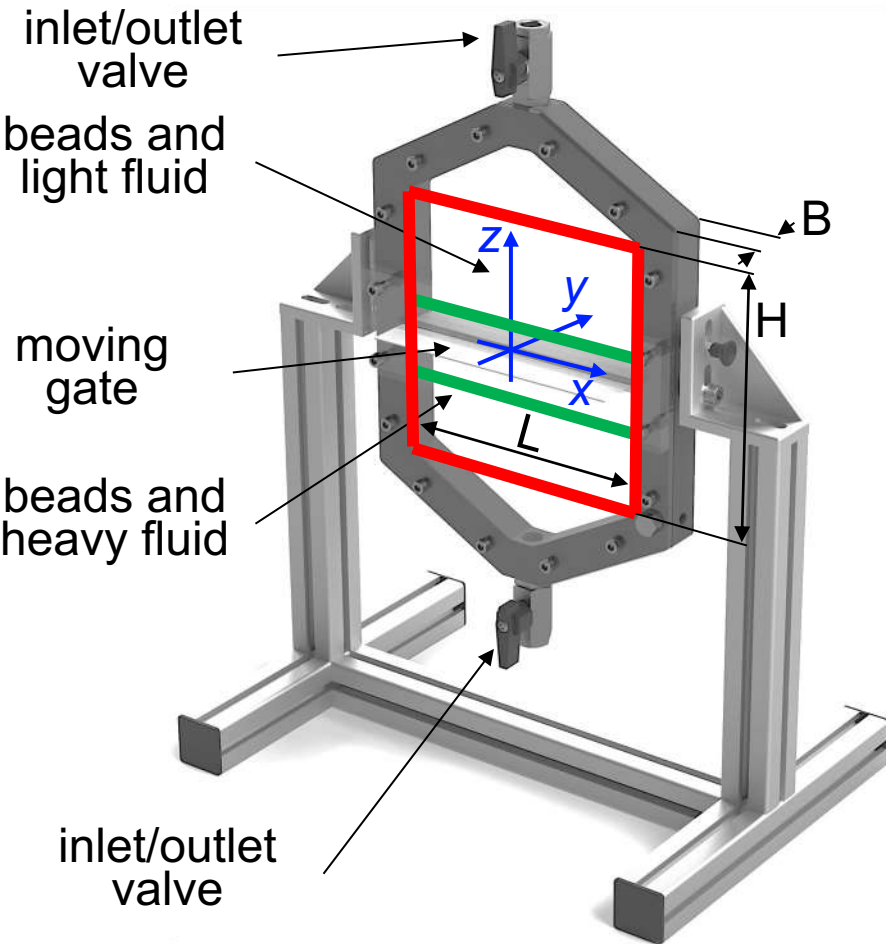
simulations



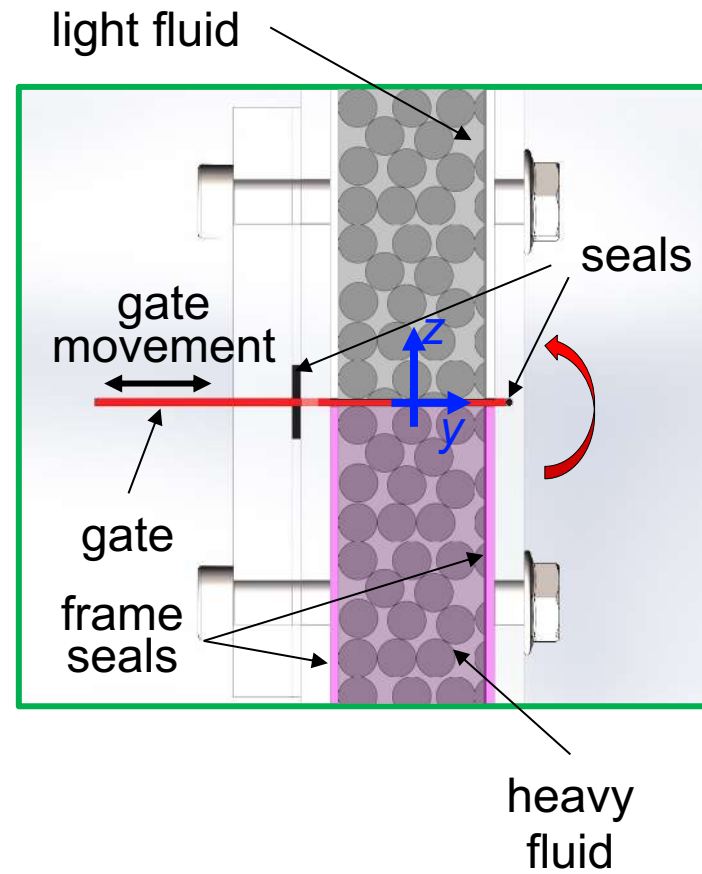
- High Schmidt number
- Porosity matched  $\phi = 0.37$
- Solid impermeable to solute
- Linear dependency  $\rho(C)$

# Experimental setup

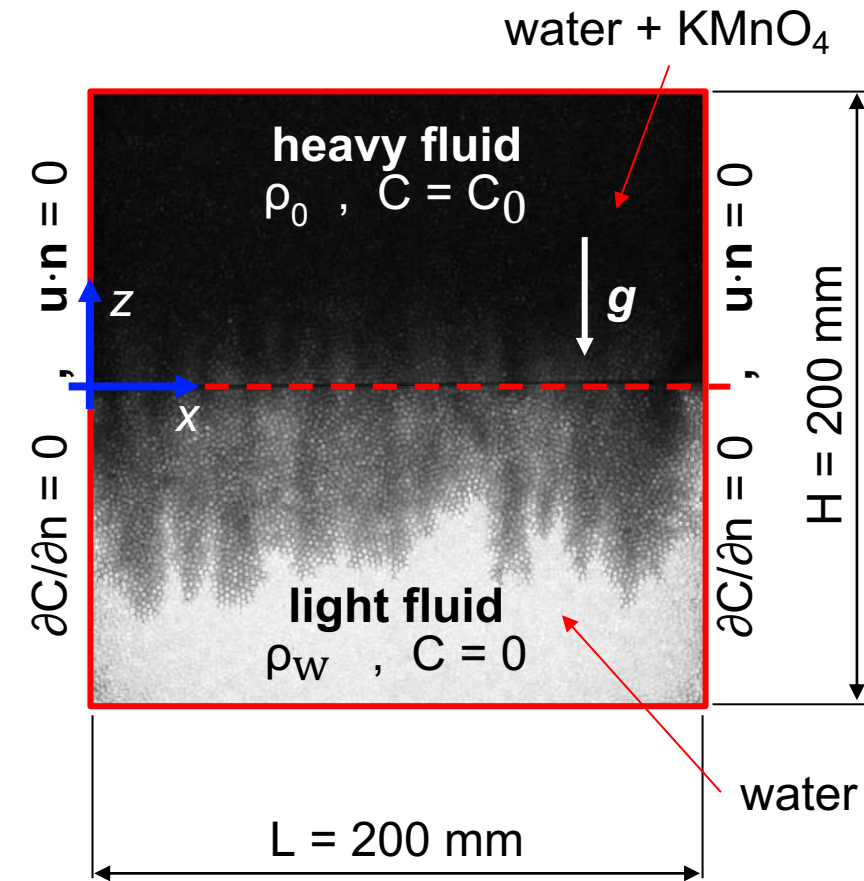
(a) Hele-Shaw cell

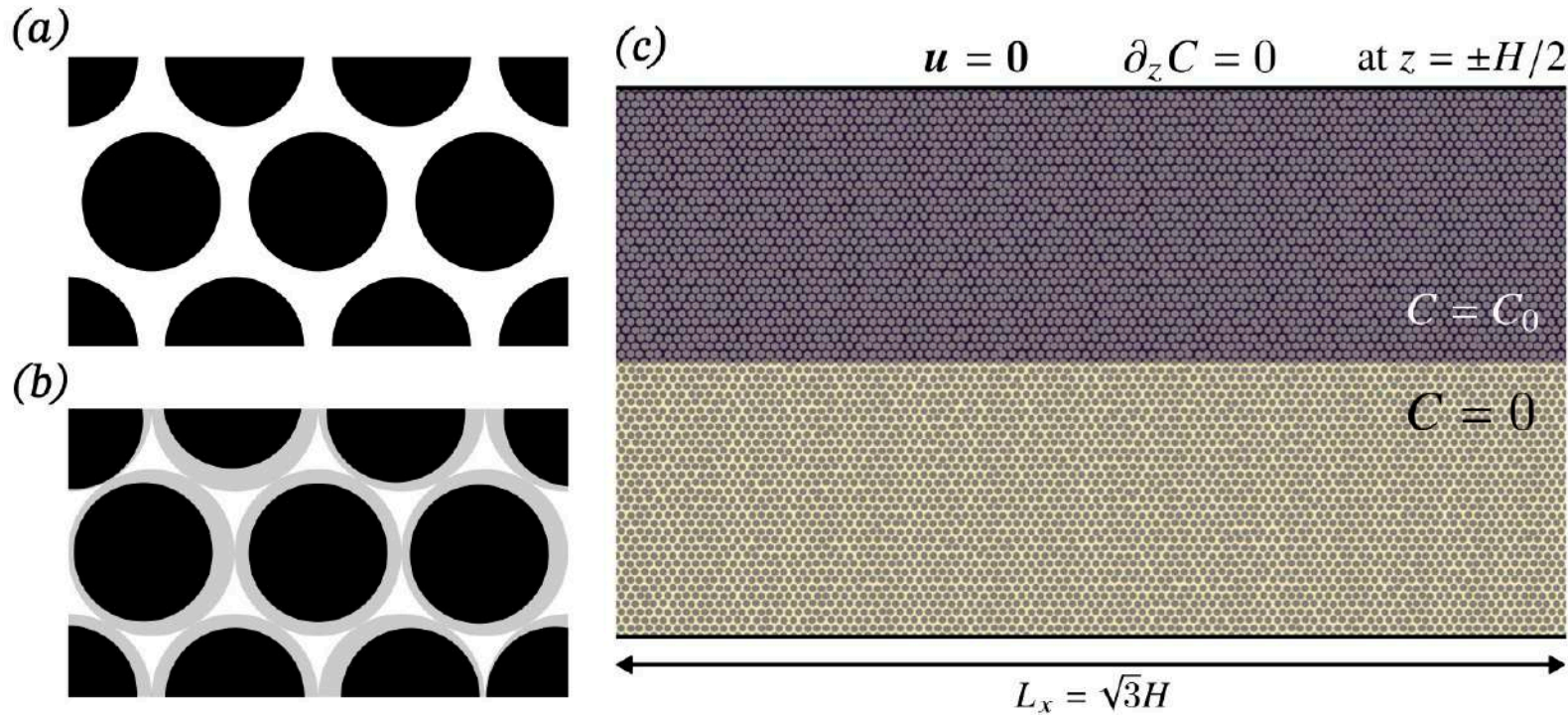


(b) gate (side view)



(c) measurement region





$$\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\rho_0^{-1} \nabla p + \nu \nabla^2 \mathbf{u} - g\beta C \hat{\mathbf{z}},$$

$$\partial_t C + (\mathbf{u} \cdot \nabla) C = D \nabla^2 C,$$

$$\rho = \rho_0 \left[ 1 + \frac{\Delta \rho}{\rho_0 C_0} (C - C_0) \right]$$

Advanced finite  
difference (AFiD,  
open source)  
+  
Immersed  
Boundaries Method

Resolution:

- velocity:  $\geq 32$  points per diameter
- concen.:  $\geq 128$  points per diameter

# Characterization of the medium

## experiments

Name	$H/d$	$\phi$	$Sc$	$Ra$	$Ra_d$	$Ra^*$	$Pe$	$Re$
E1	200	0.37	558	$4.535 \times 10^{10}$	$5.669 \times 10^3$	$2.173 \times 10^3$	0.289	0.0005
E2	200	0.37	558	$9.099 \times 10^{10}$	$1.137 \times 10^4$	$4.359 \times 10^3$	0.580	0.0010
E3	200	0.37	558	$1.824 \times 10^{11}$	$2.280 \times 10^4$	$8.737 \times 10^3$	1.163	0.0021
E4	200	0.37	558	$3.637 \times 10^{11}$	$4.546 \times 10^4$	$1.742 \times 10^4$	2.320	0.0042
E5	114	0.37	558	$4.667 \times 10^{10}$	$3.126 \times 10^4$	$6.846 \times 10^3$	1.595	0.0029
E6	114	0.37	558	$9.099 \times 10^{10}$	$6.096 \times 10^4$	$1.335 \times 10^4$	3.110	0.0056
E7	114	0.37	558	$1.820 \times 10^{11}$	$1.219 \times 10^5$	$2.671 \times 10^4$	6.222	0.0112
E8	114	0.37	558	$3.626 \times 10^{11}$	$2.429 \times 10^5$	$5.320 \times 10^4$	12.395	0.0222
E9	67	0.35	558	$4.490 \times 10^{10}$	$1.515 \times 10^5$	$1.627 \times 10^4$	5.795	0.0104
E10	67	0.35	558	$9.495 \times 10^{10}$	$3.204 \times 10^5$	$3.441 \times 10^4$	12.256	0.0220
E11	67	0.35	558	$1.834 \times 10^{11}$	$6.189 \times 10^5$	$6.646 \times 10^4$	23.672	0.0425
E12	67	0.35	558	$3.670 \times 10^{11}$	$1.239 \times 10^6$	$1.330 \times 10^5$	47.370	0.0850
E13	50	0.37	558	$4.506 \times 10^{10}$	$3.605 \times 10^5$	$3.454 \times 10^4$	18.393	0.0330
E14	50	0.37	558	$9.101 \times 10^{10}$	$7.281 \times 10^5$	$6.976 \times 10^4$	37.150	0.0666
E15	50	0.37	558	$1.824 \times 10^{11}$	$1.460 \times 10^6$	$1.398 \times 10^5$	74.474	0.1336
E16	50	0.37	558	$3.622 \times 10^{11}$	$2.898 \times 10^6$	$2.777 \times 10^5$	147.861	0.2652

## flow scales and parameters

$$k = \frac{d^2}{36k_C} \frac{\phi^3}{(1-\phi)^2} \quad U = \frac{g\Delta\rho k}{\mu} \quad \ell = \frac{\phi D}{U} \quad Sc = \frac{\mu}{\rho_0 D}$$

## simulations

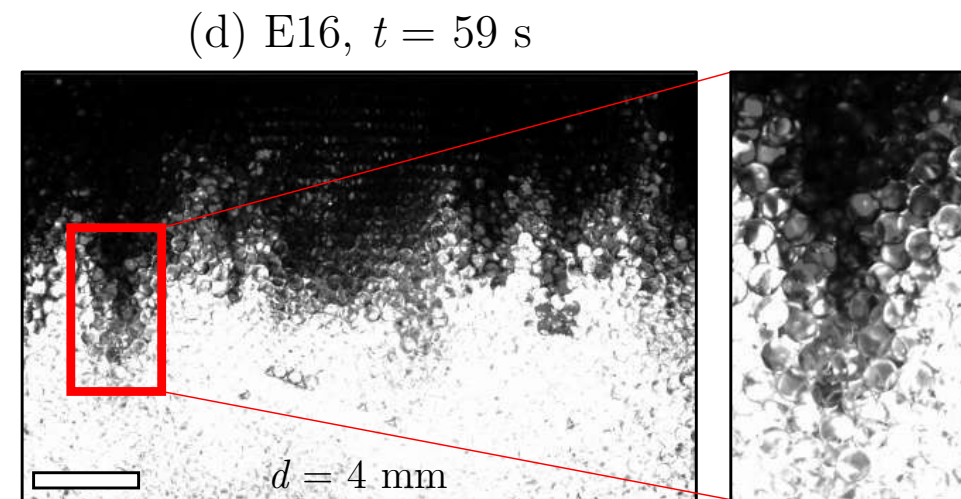
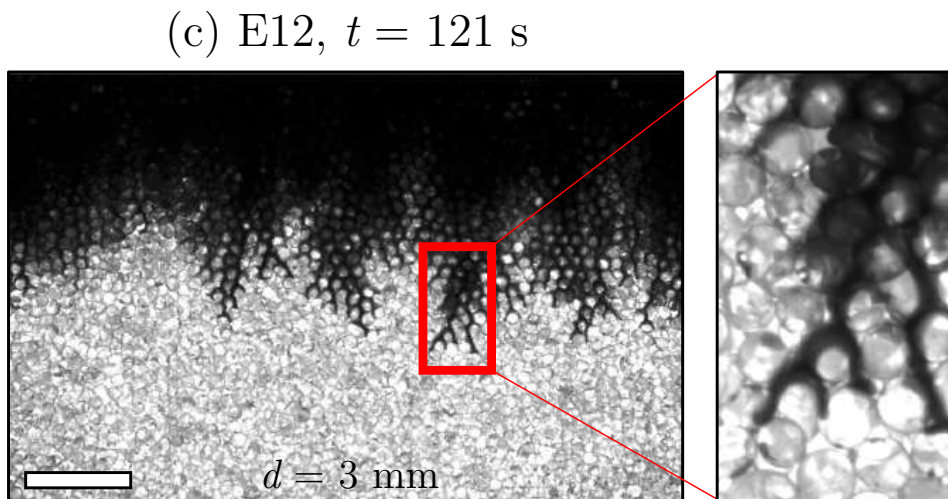
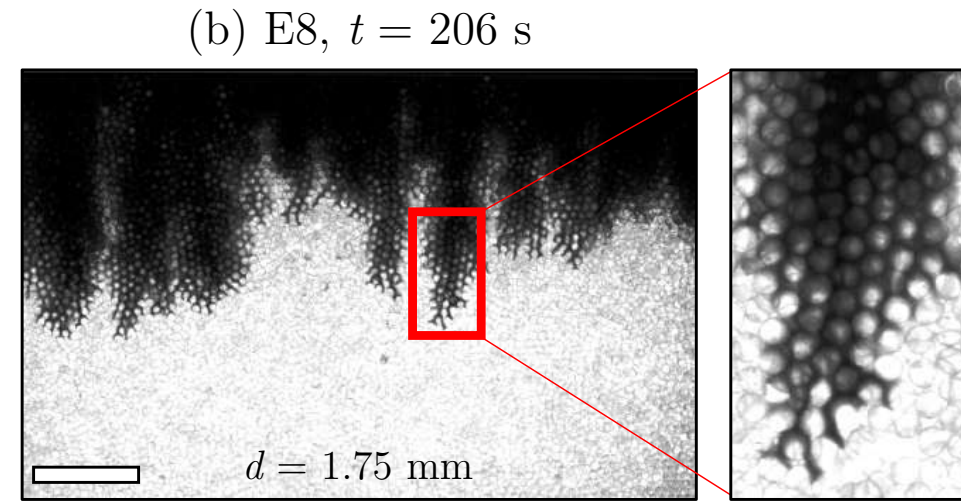
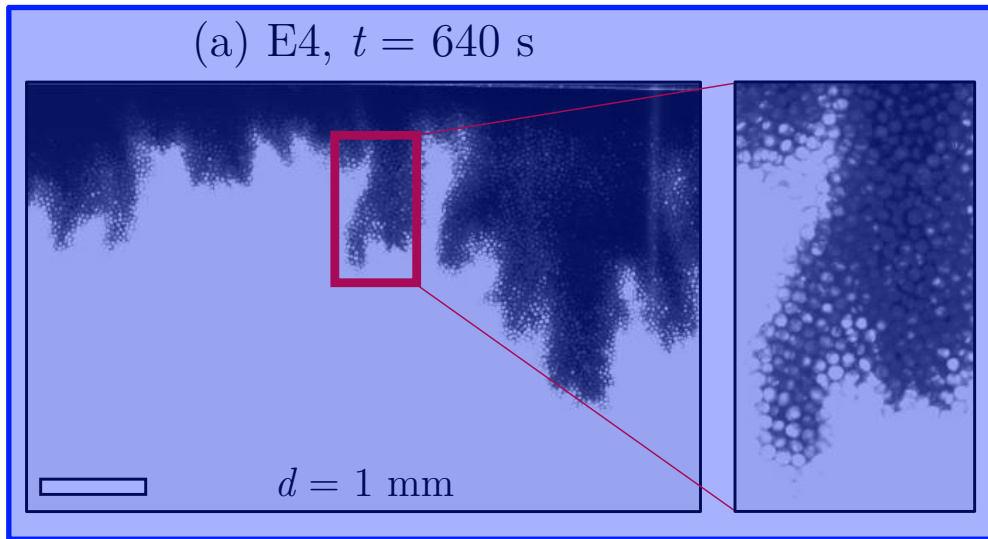
Name	$H/d$	$\phi$	$Sc$	$Ra$	$Ra_d$	$Ra^*$	$Pe$	$Re$
S1	17	0.37	100	$5.268 \times 10^8$	$1.000 \times 10^5$	$3.334 \times 10^3$	5.102	0.0510
S2	17	0.37	100	$1.666 \times 10^9$	$3.162 \times 10^5$	$1.054 \times 10^4$	16.135	0.1614
S3	17	0.37	100	$5.268 \times 10^9$	$1.000 \times 10^6$	$3.334 \times 10^4$	51.024	0.5102
S4	35	0.37	100	$4.214 \times 10^9$	$1.000 \times 10^5$	$6.669 \times 10^3$	5.102	0.0510
S5	35	0.37	100	$1.333 \times 10^{10}$	$3.162 \times 10^5$	$2.109 \times 10^4$	16.135	0.1614
S6	35	0.37	100	$4.214 \times 10^{10}$	$1.000 \times 10^6$	$6.669 \times 10^4$	51.024	0.5102
S7	52	0.37	100	$1.422 \times 10^{10}$	$1.000 \times 10^5$	$1.000 \times 10^4$	5.102	0.0510
S8	52	0.37	100	$4.498 \times 10^{10}$	$3.162 \times 10^5$	$3.163 \times 10^4$	16.135	0.1614
S9	52	0.37	100	$1.422 \times 10^{11}$	$1.000 \times 10^6$	$1.000 \times 10^5$	51.024	0.5102
S10	70	0.37	100	$3.372 \times 10^{10}$	$1.000 \times 10^5$	$1.334 \times 10^4$	5.102	0.0510
S11	70	0.37	100	$1.066 \times 10^{11}$	$3.162 \times 10^5$	$4.218 \times 10^4$	16.135	0.1614
S12	70	0.37	100	$3.372 \times 10^{11}$	$1.000 \times 10^6$	$1.334 \times 10^5$	51.024	0.5102

## dimensionless parameters

$$Da = k/H^2 \quad Ra = \frac{g\Delta\rho H^3}{\mu D} \quad Ra_d = \frac{g\Delta\rho d^3}{\mu D}$$

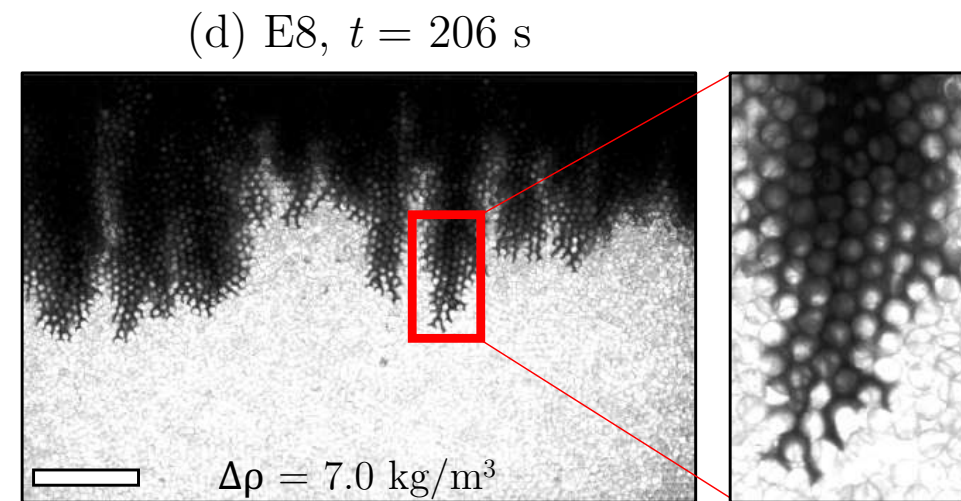
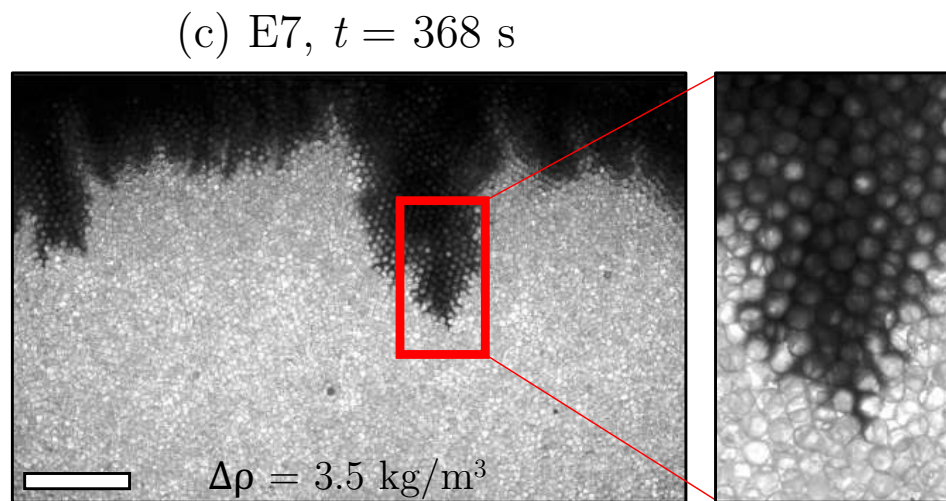
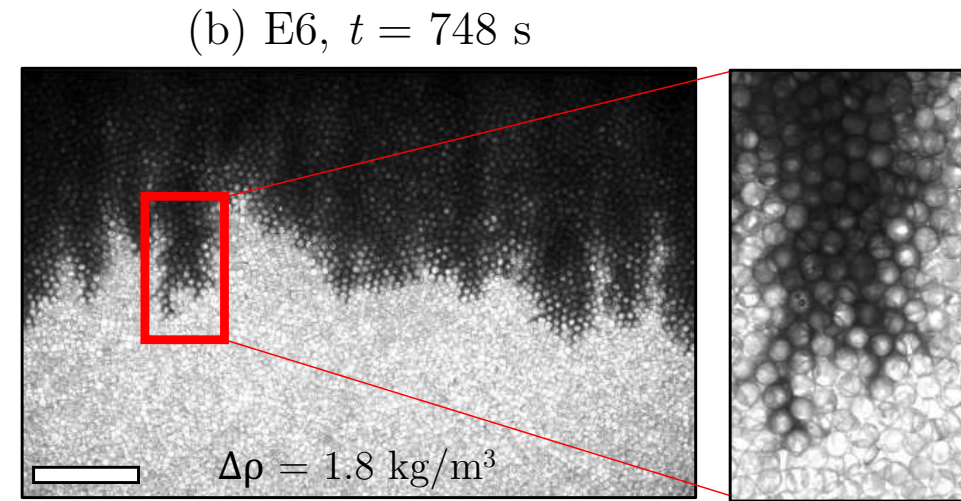
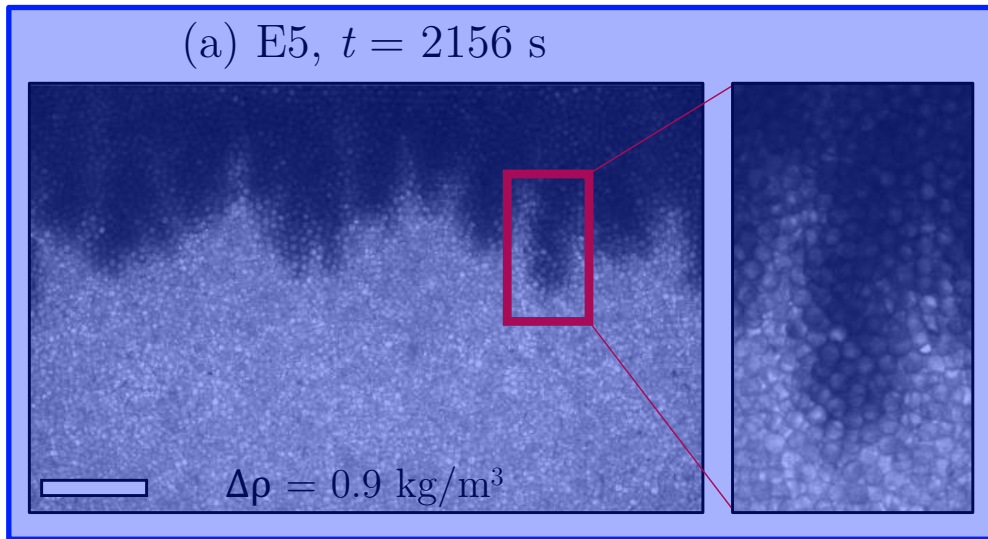
$$Ra^* = \frac{Ra Da}{\phi} \quad Re = \frac{Ra^* Da^{1/2}}{Sc} \quad Pe = Ra^* Da^{1/2}$$

# Influence of $d$ ( $\Delta\rho = 7 \text{ kg/m}^3$ )

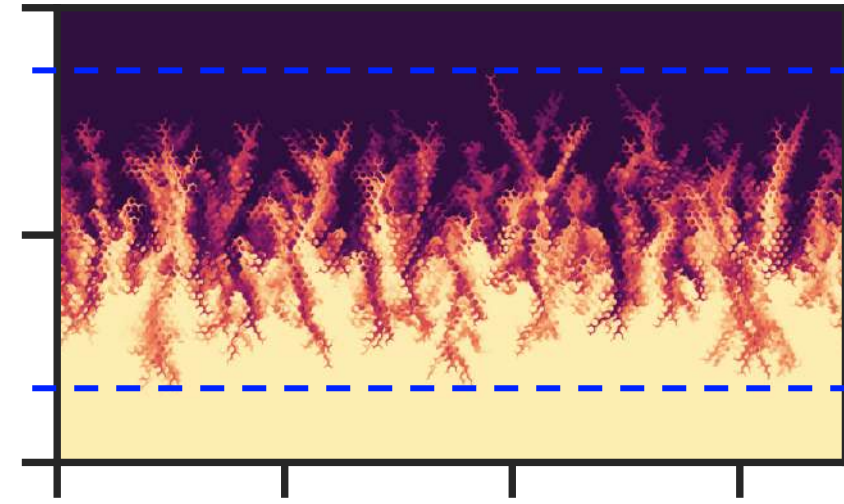




# Influence of $\Delta\rho$ ( $d = 1.75$ mm)



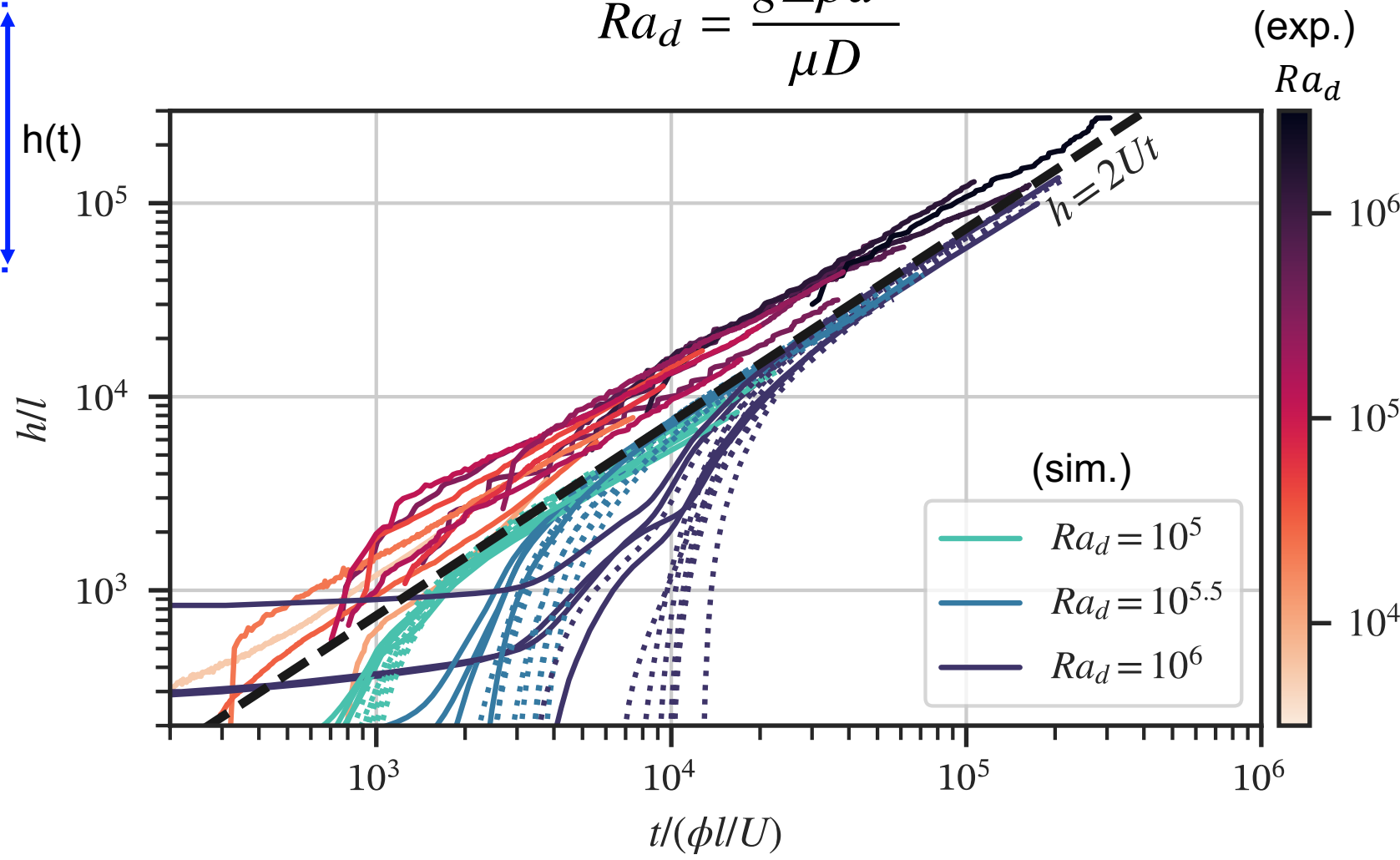
# Mixing length



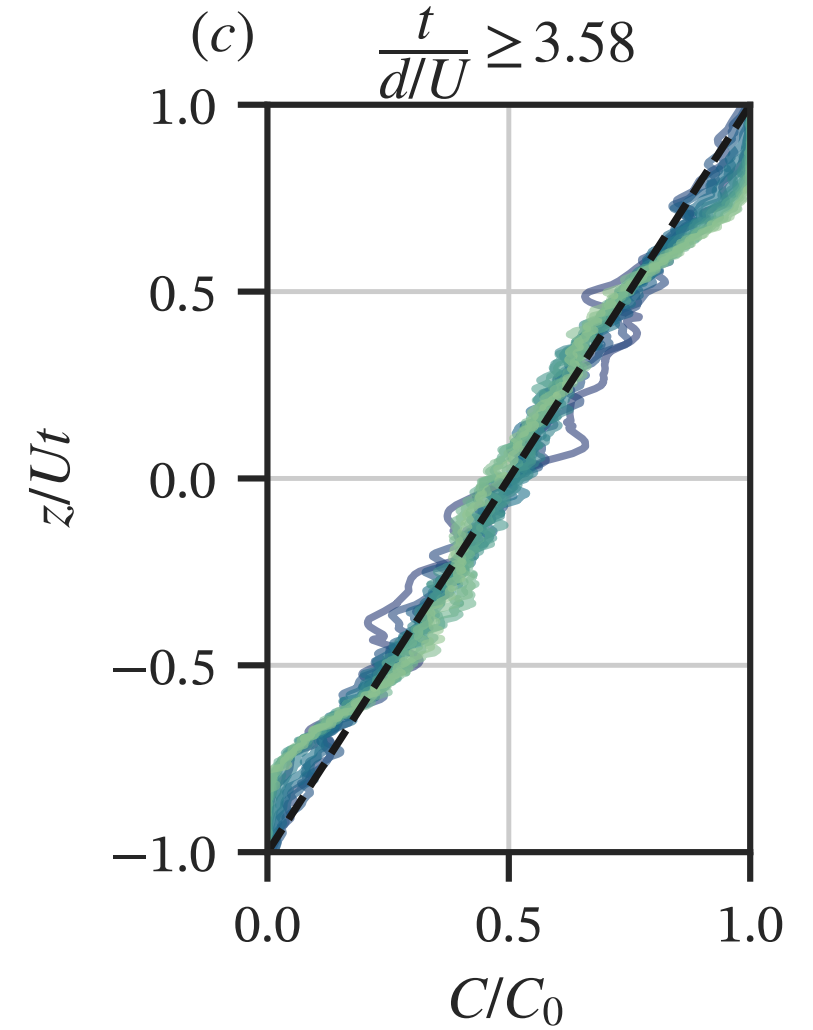
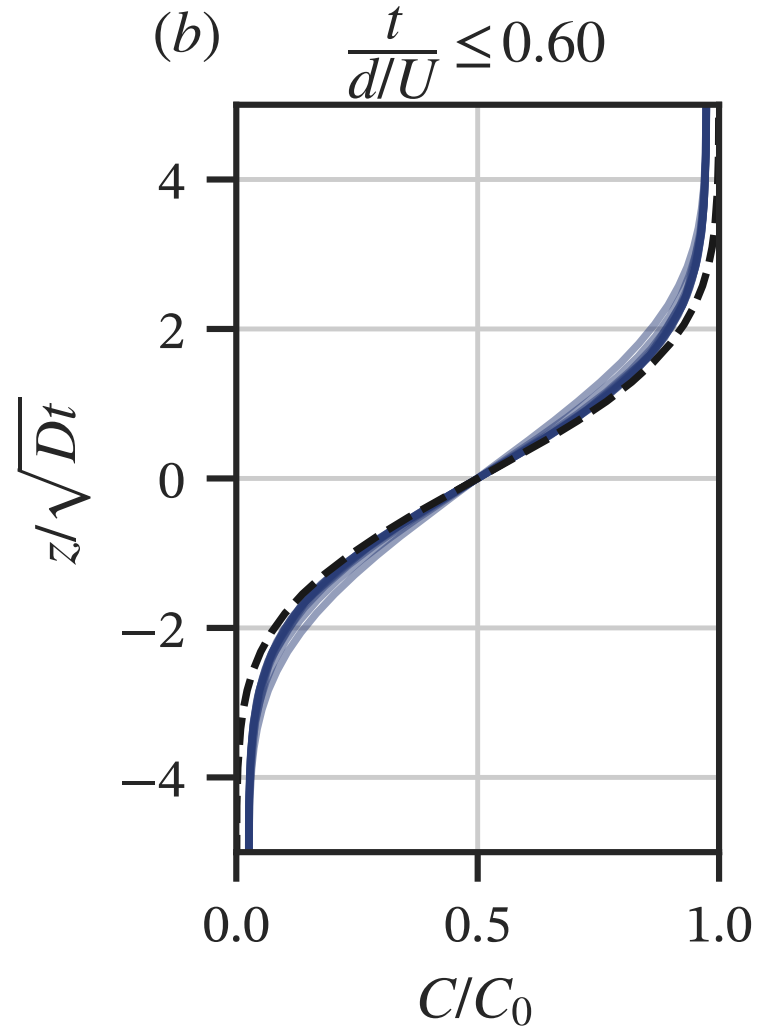
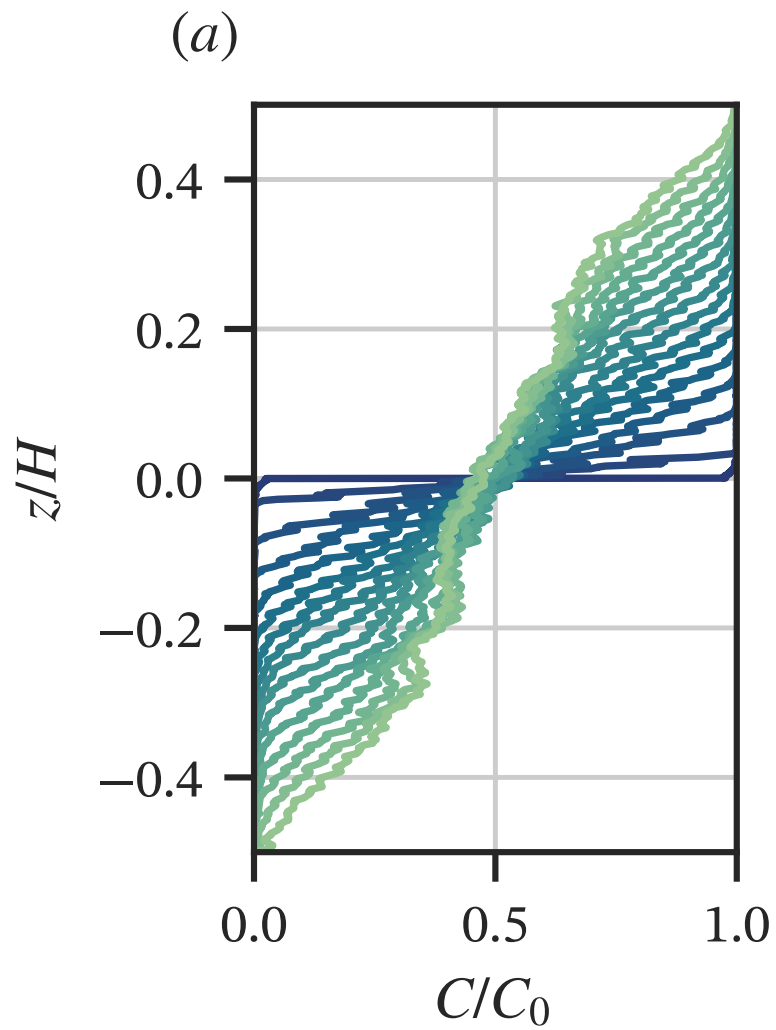
$$U = \frac{g\Delta\rho k}{\mu}$$

$$\ell = \frac{\phi D}{U}$$

$$Ra_d = \frac{g\Delta\rho d^3}{\mu D}$$



# Concentration profiles



$$\chi = D \langle |\nabla C|^2 \rangle_f = \frac{D}{V_f} \int_{V_f} |\nabla C|^2 dV$$

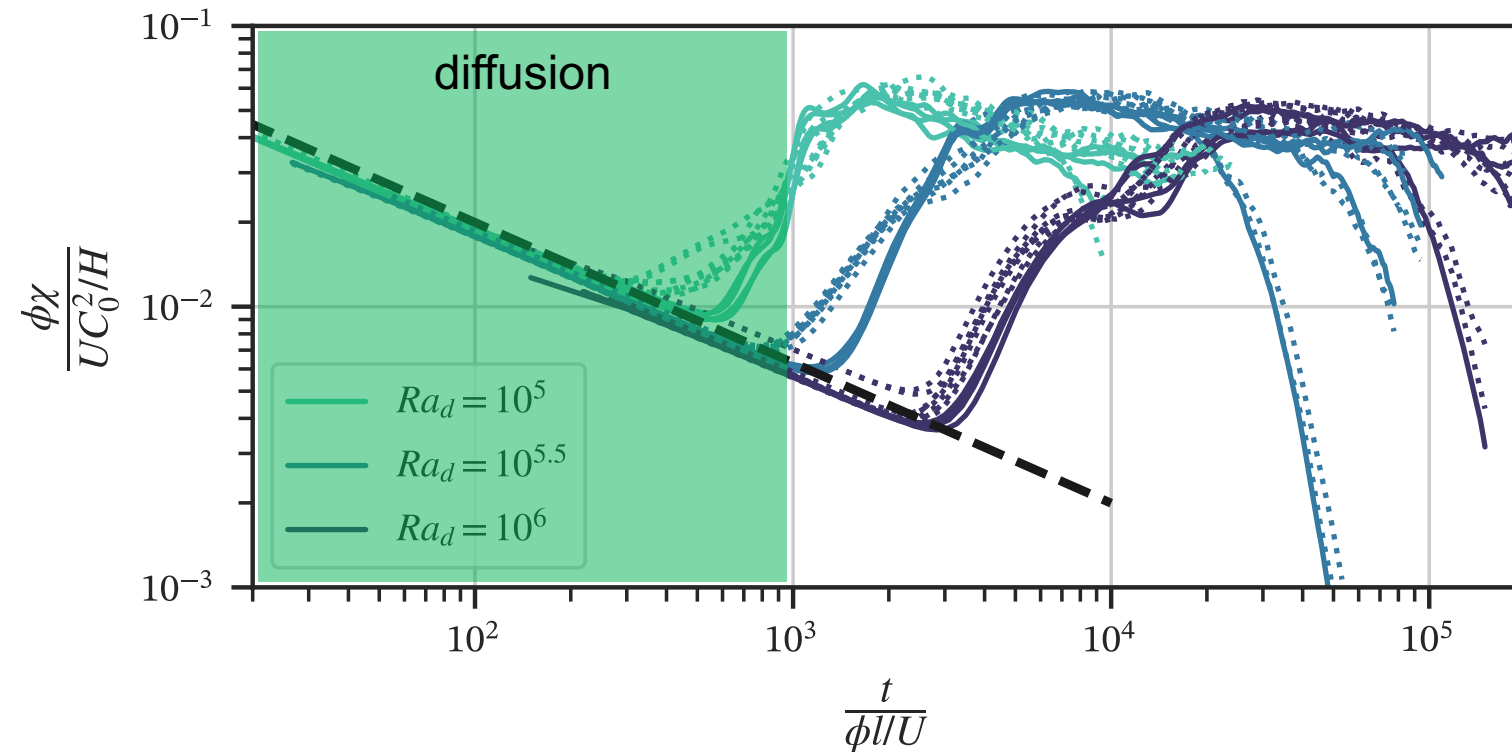
Can we model this mixing/dissolution process?

Diffusion:

$$C = C_0 + \frac{\Delta C}{2} \operatorname{erf} \left( \frac{z}{\sqrt{2\kappa t}} \right)$$

$$\partial_z C = \frac{\Delta C}{2\sqrt{\pi\kappa t}} \exp \left( -\frac{z^2}{2\kappa t} \right)$$

$$\begin{aligned} \chi &= \kappa \langle |\nabla C|^2 \rangle = \frac{\kappa}{H} \int_{-\infty}^{\infty} |\partial_z C|^2 dz \\ &= \sqrt{\frac{\kappa}{8\pi t}} \frac{(\Delta C)^2}{H} \end{aligned}$$



# Modelling scalar dissipation

$$\chi = D \langle |\nabla C|^2 \rangle_f = \frac{D}{V_f} \int_{V_f} |\nabla C|^2 dV$$

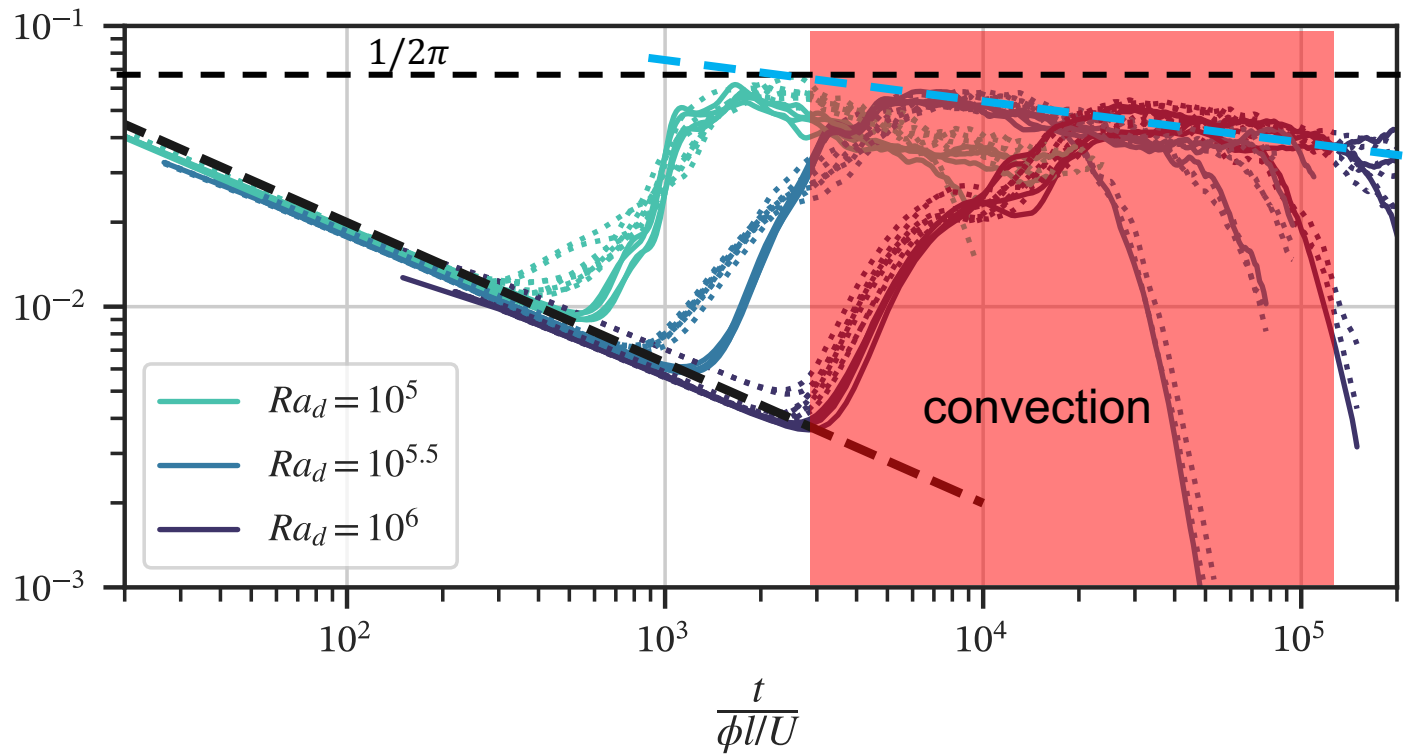
## Convection

$$\chi = \kappa \langle |\nabla C|^2 \rangle = \kappa \frac{L_m}{H} \langle |\nabla C|^2 \rangle_{ML},$$

$$|\nabla C| \approx \frac{\Delta C}{2\sqrt{\pi \kappa t}}$$

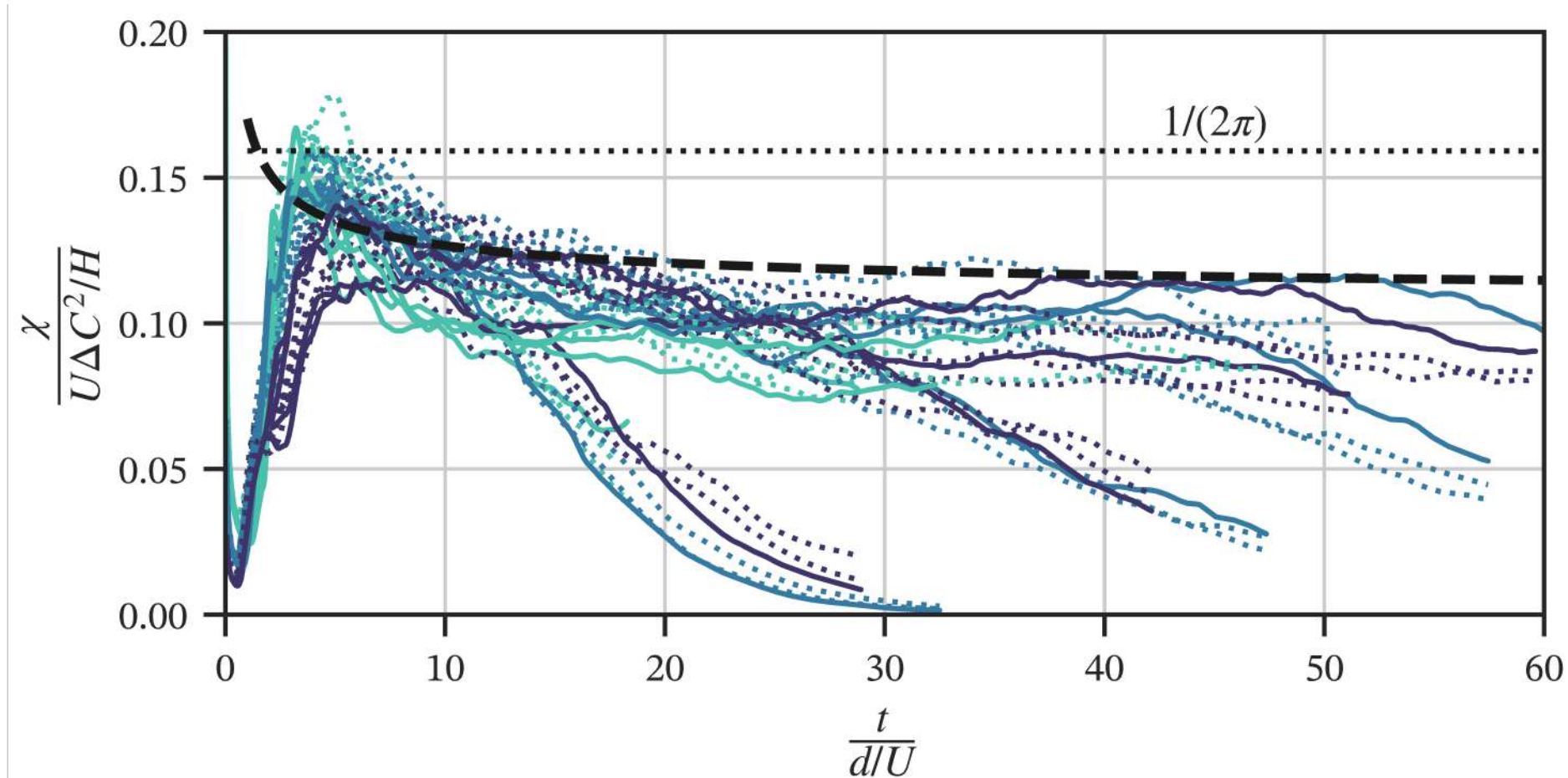
$$L_m \approx 2Ut,$$

$$\chi \approx \kappa \frac{2Ut}{H} \frac{(\Delta C)^2}{4\pi \kappa t} = \frac{1}{2\pi} \frac{U_d (\Delta C)^2}{H}$$



$1/2\pi$  is the maximum value of dissipation. Practically,  $\chi$  decreases with time

# Modelling scalar dissipation

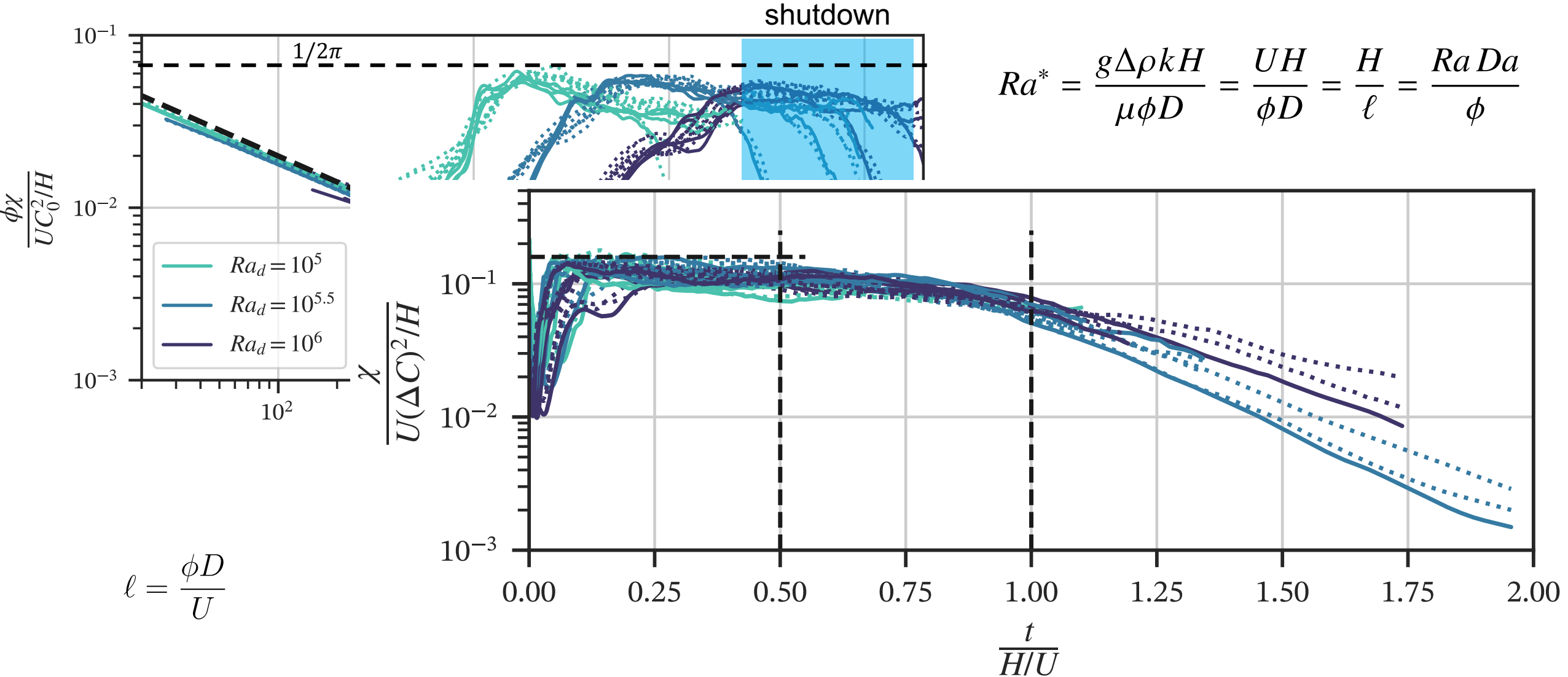


$1/2\pi$  is the maximum value of dissipation.

Model shown starting from  $t/(d/U) = 1$ . Time is also increased by  $d/U$  to account for initial condition.

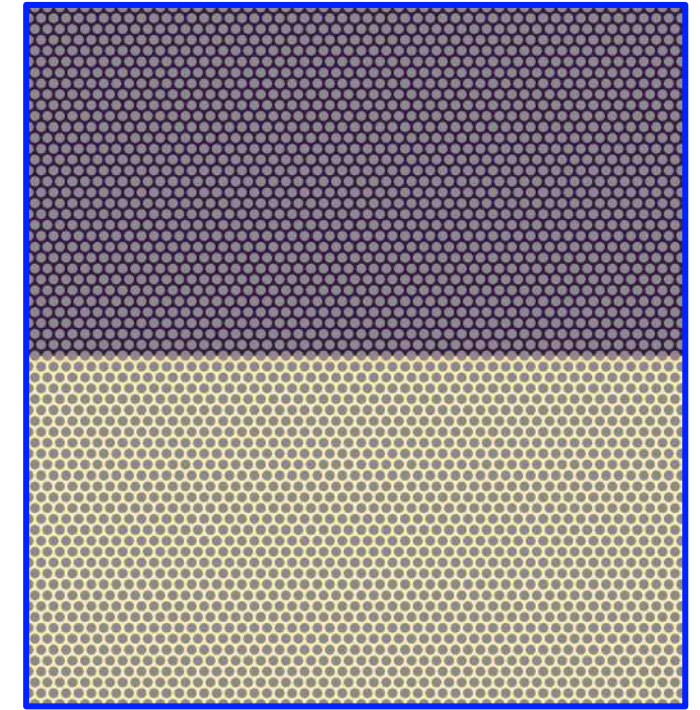
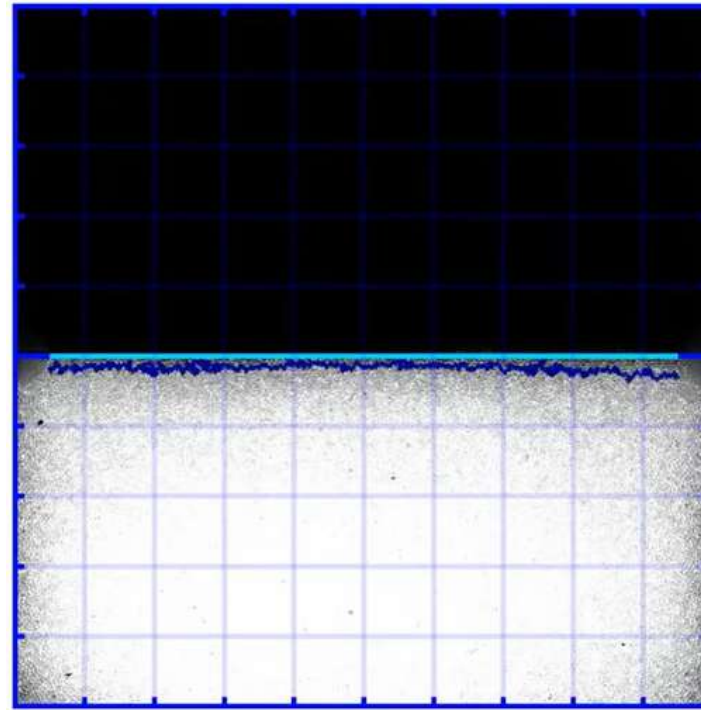
$$\frac{\chi(t=1)}{(\Delta C)^2 U / H} = \frac{\beta}{\alpha \pi} \left(1 + \frac{\alpha}{4}\right) \approx \frac{1}{1.92\pi} \approx \frac{1}{2\pi}$$

# Modelling scalar dissipation



# Conclusions

- Simulations and experiments are used as complementary tools to investigate convection in porous media
- Multiple length scales are relevant at different phases of the process
- Mixing length predicted experimentally exhibits a self-similar behaviour that agrees well with theoretical prediction for convective flows in porous media
- Mixing measured numerically via mean scalar dissipation has a self-similar behaviour.
- We explain theoretically the scaling laws observed
- We plan to expand the parameters space investigated and performed simulations in three-dimensional domains

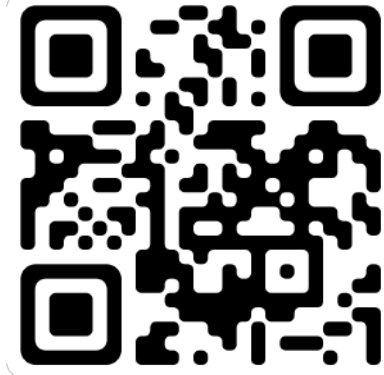


FWF

Der Wissenschaftsfonds.

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**Thank you for your attention! Questions?**





High-resolution images, movies and slides are available upon request to [m.depaoli@utwente.nl](mailto:m.depaoli@utwente.nl)